

AMENDMENTS TO THE SPECIFICATION

Please amend the specification as follows:

Amend the paragraph beginning on page 89, line 18 as follows:

A solution was prepared by dissolving 10 mg of the product a raw material in 1 g of CDCl₃. A ¹H-NMR of the solution thus prepared was measured at room temperature with the use of an NMR measurement apparatus (Gemini-300; manufactured by Varian Inc.). In the spectrum thus obtained, an integrated intensity assigned to aromatic protons and an integrated intensity assigned to aliphatic protons were observed. The styrene content was determined in accordance with the ratio of (i) the integrated intensity assigned to the aromatic protons to (ii) the integrated intensity assigned to the aliphatic protons.

Amend the paragraph beginning on page 93, line 7 as follows:

Table 1 shows the imidization ratio[[],] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material. FIG. 1 shows the IR spectrum of the imide resin. Further, the imide resin has a melt viscosity of 16000 poise.

Amend the paragraph beginning on page 93, line 21 as follows:

Table 1 shows the imidization ratio[[],] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 94, line 8 as follows:

Table 1 shows the imidization ratio[[],] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 95, line 11 as follows:

The imide resin thus obtained has an imidization ratio of 66%[[],] and a glass transition temperature of 151° C[[], and]]. The raw material has a styrene content of 20%.

Amend the paragraph beginning on page 95, line 23 as follows:

Table 1 shows the imidization ratio[[],] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 96, line 5 as follows:

An imide resin was produced by imidizing (i) a commercially available methyl methacrylate-styrene copolymer (Estyrene MS-800; manufactured by Nippon Steel Chemical Co., Ltd.) with the use of (ii) monomethylamine serving as an imidization agent. The extruder used herein is an intermeshing co-rotating type twin-screw extruder having a bore diameter of 15 mm. The temperature of temperature control zones of the extruder was set at 230°C. The screw rotation speed was set at 300 rpm. The poly(methyl methacrylate)-styrene copolymer was fed to the extruder at a feed rate of 1 kg/hr, and monomethylamine was fed in 20 parts by weight

of the poly(methyl methacrylate)-styrene copolymer. The poly(methyl methacrylate)-styrene copolymer was fed through a hopper of the extruder, and was melted in a kneading block of the extruder such that the kneading block was fully charged with the resin thus melted. Thereafter, monomethylamine was injected through a nozzle of the extruder. A seal ring was placed in an end of the reaction zone such that the reaction zone was fully charged with the resin. After the reaction, a by-product and an excess of methylamine were volatilized while reducing the pressure exerted on a vent of the extruder to -0.02 MPa. The imide resin was extruded through a die provided at an exit of the extruder, so as to be shaped into a strand. The imide resin thus extruded was cooled down in a water tank, and then was pelletized by a pelletizer. Table 1 shows the imidization ratio[[,]] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 97, line 17 as follows:

Table 1 shows the imidization ratio[[,]] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 98, line 4 as follows:

Table 1 shows the imidization ratio[[,]] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 98, line 16 as follows:

Table 1 shows the imidization ratio[[],] and glass transition temperature of the imide resin thus obtained, and styrene content of the ~~imide resin thus obtained~~ raw material.

Amend the paragraph beginning on page 99, line 6 as follows:

Table 1 shows the imidization ratio[[],] and glass transition temperature of the imide resin thus obtained, and styrene content of the ~~imide resin thus obtained~~ raw material.

Amend the paragraph beginning on page 99, line 17 as follows:

Table 1 shows the imidization ratio[[],] and glass transition temperature of the imide resin thus obtained, and styrene content of the ~~imide resin thus obtained~~ raw material.

Amend the paragraph beginning on page 100, line 20 as follows:

The imide resin thus obtained has an imidization ratio of 56%[[],] and a glass transition temperature of 131° C[[], and]]. The raw material has a styrene content of 40%.

Amend the paragraph beginning on page 102, line 5 as follows:

Table 1 shows the imidization ratio, glass transition temperature, ~~styrene content~~, total light transmittance, turbidity, and orientation birefringence of the imide resin thus obtained and styrene content of the raw material. FIG. 1 shows the IR spectrum of the imide resin.

Amend the paragraph beginning on page 103, line 10 as follows:

The imide resin thus obtained has an imidization ratio of 67%, and a glass transition temperature of 158°C[, and]]. The raw material has a styrene content of 10%.

Amend the paragraph beginning on page 106, line 15 as follows:

An NMR measurement apparatus (Gemini-300; manufactured by Varian Inc.) was used. The styrene content of the raw material was determined in accordance with the ratio of (i) an integrated intensity assigned to aromatic protons to (ii) an integrated intensity assigned to aliphatic protons.

Amend the paragraph beginning on page 110, line 6 as follows:

Table 3 shows the imidization ratio[,,] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 111, line 19 as follows:

Table 3 shows the imidization ratio[,,] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 112, line 9 as follows:

Table 1 shows the imidization ratio, glass transition temperature[[],] and total light transmittance of the resin thus obtained, and an amount of styrene of the ~~resin thus obtained~~ raw material.

Amend the paragraph beginning on page 114, line 16 as follows:

An imide resin was produced by imidizing (i) a commercially available methyl methacrylate-styrene copolymer (Estyrene MS-800; manufactured by Nippon Steel Chemical Co., Ltd.) with the use of (ii) methylamine serving as an imidization agent. The extruder used herein is an intermeshing co-rotating type twin-screw extruder having a bore diameter of 15 mm. The temperature of temperature control zones of the extruder was set at 230.degree. C. The screw rotation speed was set at 300 rpm. The MS resin was fed to the extruder at a feed rate of 0.75 kg/hr, and methylamine was fed in 40 parts by weight of the MS resin. The MS resin was fed through a hopper of the extruder, and was melted in a kneading block of the extruder such that the kneading block was fully charged with the resin thus melted. Thereafter, methylamine was injected through a nozzle of the extruder. A seal ring was placed in an end of the reaction zone such that the reaction zone was fully charged with the resin. After the reaction, a by-product and an excess of methylamine were volatilized while reducing the pressure exerted on a vent of the extruder to -0.02 MPa. The imide resin was extruded through a die provided at an exit of the extruder, so as to be shaped into a strand. The imide resin thus extruded was cooled down in a

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water tank, and then was pelletized by a pelletizer. Table 5 shows the imidization ratio[[],] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 116, two lines up from the bottom as follows:

In Example 19, the same operations were carried out as in Example 18, except that the MS resin was fed at a feed rate of 1.0 kg/hr. Table 5 shows the imidization ratio[[],] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 117, line 15 as follows:

In Comparative Example 4, the same operations were carried out as in Example 19, except that methylamine was fed in 30 parts by weight of the MS resin. Table 5 shows the imidization ratio[[],] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 118, line 4 as follows:

In Comparative Example 5, the same operations were carried out as in Example 19, except that a commercially available methyl methacrylate-styrene copolymer (Estyrene MS-600; manufactured by Nippon Steel Chemical Co., Ltd.) was used as the methyl methacrylate-styrene

copolymer and methylamine was fed in 30 parts by weight of the methyl methacrylate-styrene copolymer. Table 5 shows the imidization ratio[[,]] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 121, line 13 as follows:

An NMR measurement apparatus (Gemini-300; manufactured by Varian Inc.) was used. The styrene content of the raw material was determined in accordance with the ratio of (i) an integrated intensity assigned to aromatic protons to (ii) an integrated intensity assigned to aliphatic protons.

Amend the paragraph beginning on page 124, line 8 as follows:

An imide resin was produced by imidizing (i) a commercially available methyl methacrylate-styrene copolymer (Estyrene MS-600; manufactured by Nippon Steel Chemical Co., Ltd.) with the use of (ii) monomethylamine serving as an imidization agent. The extruder used herein is an intermeshing co-rotating type twin-screw extruder having a bore diameter of 15 mm. The temperature of temperature control zones of the extruder was set at 230°C. The screw rotation speed was set at 300 rpm. The MS resin was fed to the extruder at a feed rate of 1 kg/hr, and methylamine was fed in 30 parts by weight of the MS resin. The MS resin was fed through a hopper of the extruder, and was melted in a kneading block of the extruder such that the kneading block was fully charged with the resin thus melted. Thereafter, methylamine was injected through a nozzle of the extruder. A seal ring was placed in an end of the reaction zone

such that the reaction zone was fully charged with the resin. After the reaction, a by-product and an excess of methylamine were volatilized while reducing the pressure exerted on a vent of the extruder to -0.02 MPa. The imide resin was extruded through a die provided at an exit of the extruder, so as to be shaped into a strand. The imide resin thus extruded was cooled down in a water tank, and then was pelletized by a pelletizer. Table 8 shows the imidization ratio[[],] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 126, line 9 as follows:

In Example 21, the same operations were carried out as in Example 20, except that a commercially available methyl methacrylate-styrene copolymer (Estyrene MS-800; manufactured by Nippon Steel Chemical Co., Ltd.) was used as the methyl methacrylate-styrene copolymer and methylamine was fed in 40 parts by weight of the MS resin. Table 8 shows the imidization ratio[[],] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 127, line 10 as follows:

In Example 22, the same operations carried out as in Example 21, except that a methyl methacrylate-styrene copolymer obtained by polymerizing methyl methacrylate (90 wt %) and styrene (10 wt %) by way of mass polymerization was used as the methyl methacrylate-styrene

copolymer. Table 8 shows the imidization ratio, and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 130, line 25 as follows:

An imide resin was produced by imidizing (i) a commercially available methyl methacrylate-styrene copolymer (Estyrene MS-600; manufactured by Nippon Steel Chemical Co., Ltd.) with the use of (ii) methylamine serving as an imidization agent. The extruder used herein is an intermeshing co-rotating type twin-screw extruder having a bore diameter of 15 mm. The temperature of temperature control zones of the extruder was set at 230°C. The screw rotation speed was set at 300 rpm. The MS resin was fed to the extruder at a feed rate of 1 kg/hr, and methylamine was fed in 30 parts by weight of the MS resin. The MS resin was fed through a hopper of the extruder, and was melted in a kneading block of the extruder such that the kneading block was fully charged with the resin thus melted. Thereafter, methylamine was injected through a nozzle of the extruder. A seal ring was placed in an end of the reaction zone such that the reaction zone was fully charged with the resin. After the reaction, a by-product and an excess of methylamine were volatilized while reducing the pressure exerted on a vent of the extruder to -0.02 MPa. The imide resin was extruded through a die provided at an exit of the extruder, so as to be shaped into a strand. The imide resin thus extruded was cooled down in a water tank, and then was pelletized by a pelletizer. Table 11 shows the imidization ratio[[],] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 132, line 15 as follows:

In Example 25, the same operations were carried out as in Example 24, except that methylamine was fed in 20 parts by weight of the MS resin. Table 11 shows the imidization ratio[[,]] and glass transition temperature of the resin thus obtained, and styrene content of the resin thus obtained raw material.

Amend the paragraph beginning on page 133, line 8 as follows:

In Example 26, the same operations were carried out as in Example 24, except that (i) Atrate® MS Resin MM-70 (manufactured by Nippon A&L Inc.) was used as the methyl methacrylate-styrene copolymer, that (ii) the MS resin was fed at a feed rate of 0.5 kg/hr, and that (iii) methylamine was fed in 40 parts by weight of the MS resin. Table 11 shows the imidization ratio[[,]] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.

Amend the paragraph beginning on page 134, line 4 as follows:

In Comparative Example 8, the same operations were carried out as in Example 26, except that Estyrene MS-800 manufactured by Nippon Steel Chemical Co., Ltd. was used as the methyl methacrylate-styrene copolymer. Table 11 shows the imidization ratio[[,]] and glass transition temperature of the imide resin thus obtained, and styrene content of the imide resin thus obtained raw material.